



# PRE-ASSESSMENT FOR EVALUATING the suitability of 15 2W plants to become REEF 2W

Made by UCT on 04/2020

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## D.T4.3.3



## A) INTRODUCTION AND GENERAL INFORMATION

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According to DT4.3.3. proposal Veolia with UCT contacted several WWTP operating companies in the Czech republic to collect data about WWTPs and for preparing the pre-assessment.

There were several sites reached based on the preselection and visited: Zlin, Olomouc, Ústi nad Labem, Liberec, Hradec Kralove and Teplice.

Teplice, Liberec are rejected absolutely limited free space on sites for new technologies and Usti nad Labem for uncommon properties of wastewater (high industrial water content).

As suitable there were Zlin, Olomouc and Hradec Kralove sites chosen.

### Plant 1: WWTP Zlin

- Zlin city, east part of Czech republic, WWTP is situated in a suburban area close to industrial zones between cities Zlin and Otrokovice
- The capacity of the plant is 207000 PE, the current load is 107114 PE
- Inflow parameters:

|  |                   |        |
|--|-------------------|--------|
| Total real inlet flow                      | m <sup>3</sup> /d | 21 323 |
| Inlet pollution (COD), mg/l                | mg COD/l          | 603    |
| Inlet pollution (BOD), mg/l                | mg BOD/l          | 250    |
| The average temperature of activation tank | °C                | 14.7   |

- Technology description:

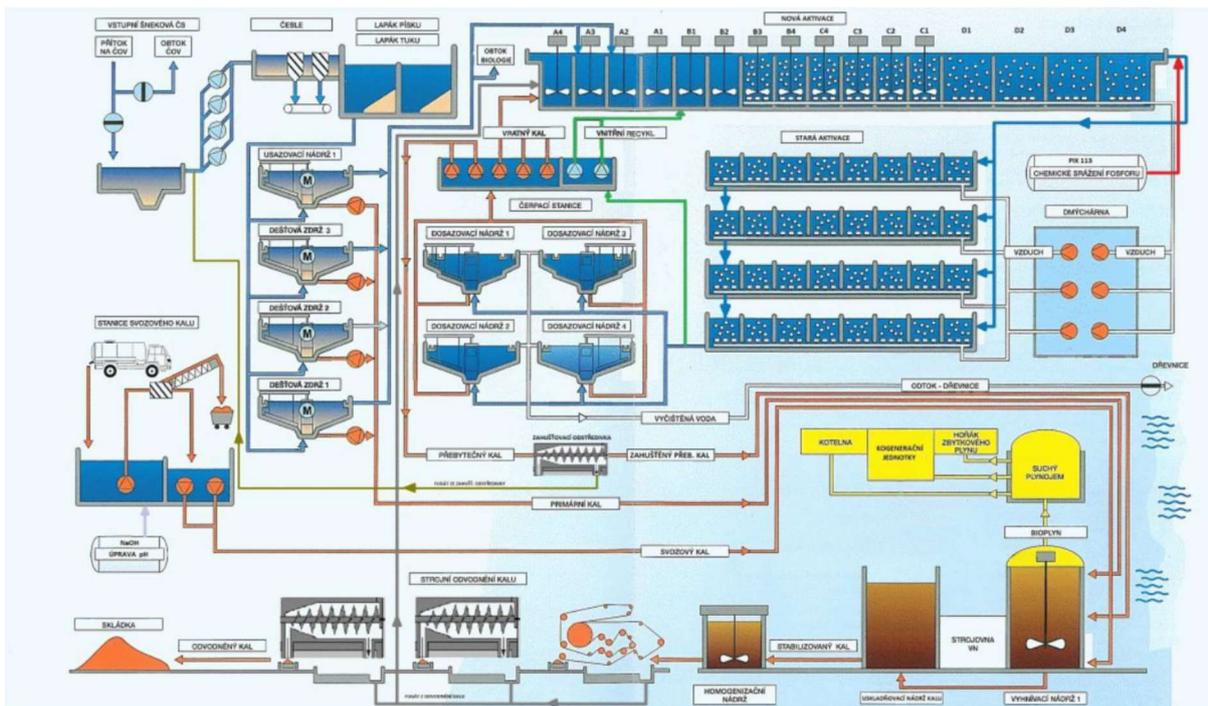
WWTP Zlin is a typical municipal mechanic-biological WWTP with primary mechanical treatment steps consisted of waste water pump station, screenings, primary sedimentation, activation with nutrient removal (optimized air distribution), round clarifiers.

The total volume of the biological treatment step: 25800 m<sup>3</sup>, treatment efficiency:

|                            |   |      |
|----------------------------|---|------|
| Efficiency COD removal     | % | 95.3 |
| Efficiency BOD removal     | % | 100  |
| Efficiency N total removal | % | 70   |
| Efficiency P total removal | % | 85   |

Sludge is thickened via thickening centrifuge and digested by AD. AD is first step with mesophilic digester 3800 m<sup>3</sup>. Distillery stillage is used as co-substrate. Biogas is used in CHP unit (gas engines) 2 x 125 kWel. Sludge is dewatered by centrifuge and used in agriculture or compost producing by external companies.

|   |          |         |
|---|----------|---------|
| Total electricity production                                  | kWh/year | 1854624 |
| Specific electricity consumption (PE - COD WWTP inlet)        | kWh/PE   | 23.8    |
| Specific electricity production (PE - COD WWTP inlet)         | kWh/PE   | 17.9    |
| Electricity self sufficiency on the basis of biogas from WWTP | %        | 75.1    |



- Operator priority is now to change sludge disposal for more sustainable technologies. Now there are developing projects for sludge drying and incineration.
- The project is chosen for pre-assessment as a very well operated plant with a responsible operator and crew with a large amount of data about operation collected and archived. There are also developing industrial zones close to the plant for RE projects.

## Plant 2: Hradec Kralove

Hradec Kralove is the regional centre of the east-central part of the Czech Republic. It is a historical city with limited industrial development. WWTP is situated close to Elbe river about 5 km outside the city. The plant is standalone without any municipal or industrial area around it. Unique is high altitude pumping station at WWTP (due to a very deep sewer system).

- Hradec Kralove city, east-central part of Czech republic, WWTP is situated in a rural area in relatively significant distance from the city and other municipalities
- The capacity of the plant is 140000 PE, the current load is 121900 PE
- Inflow parameters:

|  |                   |       |
|--|-------------------|-------|
| Total real inlet flow                  | m <sup>3</sup> /d | 33089 |
| Inlet pollution (COD), mg/l            | mg COD/l          | 442   |
| Inlet pollution (BOD), mg/l            | mg BOD/l          | 188   |
| Average temperature of activation tank | °C                | 16.0  |

- Technology description:

WWTP Hradec Kralove is a common municipal mechanic-biological WWTP with primary mechanical treatment steps consisted of waste water pump station (the deepest in CZ), screenings, primary sedimentation, activation with nutrient removal (optimized air distribution), round clarifiers. There is a tertiary biological N removal biofilter installed.

The total volume of the biological treatment step: 25975 m<sup>3</sup>, treatment efficiency:

|                            |   |      |
|----------------------------|---|------|
| Efficiency COD removal     | % | 94.5 |
| Efficiency BOD removal     | % | 99   |
| Efficiency N total removal | % | 76   |
| Efficiency P total removal | % | 89   |

Sludge is thickened via thickening centrifuge and digested by AD. AD is 2 stages with 2x mesophilic digester 4100 m<sup>3</sup>. Glycerol by-products is used as co-substrate. Biogas is used in CHP unit (gas engines) 3 x 179 kWel. Sludge is dewatered by centrifuge and used in agriculture or compost producing by external companies.

|  |          |         |
|--|----------|---------|
| Total electricity production                           | kWh/year | 3092167 |
| Specific electricity consumption (PE - COD WWTP inlet) | kWh/PE   | 46.4    |
| Specific electricity production (PE - COD WWTP inlet)  | kWh/PE   | 27.1    |
| Electricity self-sufficiency based on biogas from WWTP | %        | 58.4    |

At the plant, there is a realized project of Hazardous waste processing plant (chemical treatment plant) for liquid waste. Pretreated water from this facility is used as a co-substrate for the anaerobic digestion (COD 50 g/l).

- Operator priority is now to change sludge disposal for more sustainable technologies. Now there are developing projects for sludge drying and incineration. Also, biomethane production is now evaluated.
- The project is selected for pre-assessment as a very well operated plant with a responsible operator and crew with a large amount of data about operation collected and archived. There is a potential-free space close to the plant for development.



WWTP Olomouc is standard municipal mechanic-biological WWTP with primary mechanical treatment step consisted of waste water pump station, screenings, primary sedimentation, activation with nutrient removal (optimized air distribution), round clarifiers.

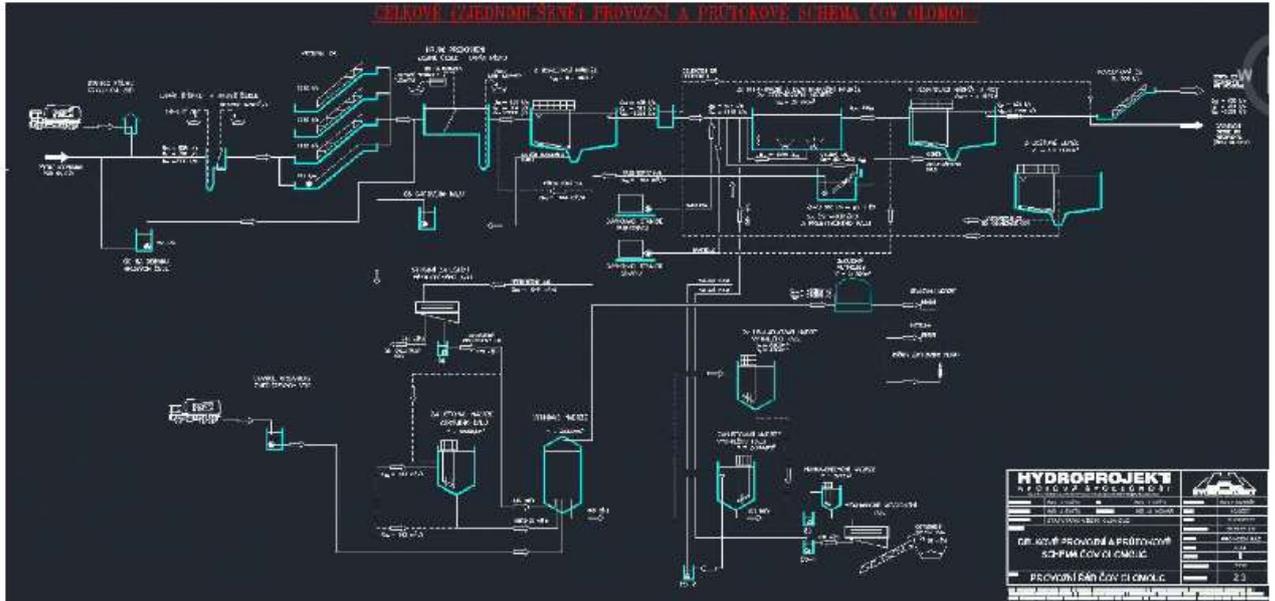
The total volume of the biological treatment step: 39 960 m<sup>3</sup>, treatment efficiency:

|                            |   |      |
|----------------------------|---|------|
| Efficiency COD removal     | % | 96.5 |
| Efficiency BOD removal     | % | 99   |
| Efficiency N total removal | % | 85   |
| Efficiency P total removal | % | 92   |

Sludge is gravity thickened and digested by AD. AD is first stage with 3x mesophilic digester 3200 m<sup>3</sup>. Lecitin wastewater is used as co-substrate. Biogas is used in CHP unit (gas engines) 2 x 450 kWel. Sludge is dewatered by centrifuge and used in agriculture or compost producing by external companies.

|  |          |         |
|--|----------|---------|
| Total electricity production                           | kWh/year | 2650197 |
| Specific electricity consumption (PE - COD WWTP inlet) | kWh/PE   | 29.0    |
| Specific electricity production (PE - COD WWTP inlet)  | kWh/PE   | 13.1    |
| Electricity self-sufficiency based on biogas from WWTP | %        | 45.3    |

- Operator priority is now to replace CHP energy center and to find a new solution for biogas - CHP, boiler with sludge dryer and biomethane unit are evaluated
- The project is chosen for pre-assessment as a very well operated plant with a responsible operator and crew with a large amount of data about operation collected and archived. The current CHP unit has to be replaced immediately because of the end of engines live-cycle. Still, there is a possibility to realize other kind of biogas use, which is suitable for using REEF2W tool.



## B) PRE-ASSESSMENT APPROACH (METHODOLOGY)

The first selection of the possible sites was based on the data provided by Veolia and information from the workshop made in December in Prague. We choose several WWTP in Zlin, Olomouc, Ústí nad Labem, Liberec, Hradec Kralove and Teplice for further investigations. Then we conduct a series of phone calls and videoconferences with selected sites according to which Teplice and Liberec were eliminated due to the limited free space. WWTP in Usti nad Labem was excluded after considering the specific pollution of wastewater due to industry in the region. The remaining sites agreed to participate in preassessment and data was obtained through the Data collection sheet from the Tool. The data provided from WWTPs were then used in the tool for evaluating energy efficiency. Each of the WWTPs was interested in the testing possibility of using biomethane at there sites. Therefore, we evaluated each of them in the same way, where we evaluated energy efficiency and then compared current and future situation when all biogas production was transferred in the biomethane.

## C) RESULTS

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### ZLIN

The plant situation was analyzed by REEF2W Tool with the following results:

| WWTP Description                 |                            |        |                     |
|----------------------------------|----------------------------|--------|---------------------|
|                                  | Status quo                 |        | Future situation    |
| Plant type                       | Wastewater Treatment Plant |        |                     |
| Name of User                     | Zlin                       |        |                     |
| Date                             | 2020/04/29                 |        |                     |
| Country                          | Czech Republic             |        |                     |
| Treatment capacity               | 207000                     | 207000 | PE (*)              |
| Connected population             | 107114                     | 107114 | PE (*)              |
| Daily average of wastewater flow | 21323                      | 21323  | m <sup>3</sup> /d   |
| COD inflow concentration         | 603                        | 603    | mg/l                |
| TN in influent                   | 49,44                      | 49,44  | kgTN/m <sup>3</sup> |

| Substrate                                 |            |                |              |
|---|------------|----------------|--------------|
| Status quo                                |            |                |              |
|   | Tons (t/y) | Tot. Solid (%) | Volatile (%) |
| Primary Sludge                            | 24727,0    | 4,5            | 76,0         |
| Secondary Sludge                          | 16113,0    | 6,0            | 40,3         |
| External Sewage Sludge                    | NA         | NA             | NA           |
| Organic Fraction of Municipal Solid Waste | NA         | NA             | NA           |
| Other                                     | 4790,0     | 6,9            | 40,0         |
| Other                                     | 200,0      | 80,0           | 80,0         |
| NA  | NA         | NA             | NA           |
| NA  | NA         | NA             | NA           |

There are no changes in substrates.

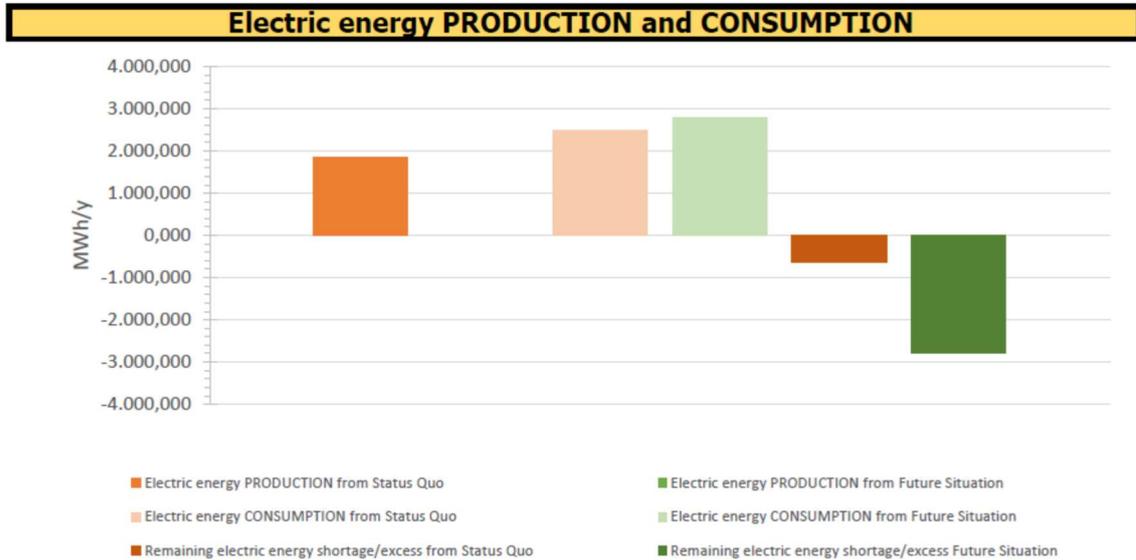
| Energy efficiency               |            |                  |                |      |            |                  |      |
|---------------------------------|------------|------------------|----------------|------|------------|------------------|------|
| WWTP Indicator                  |            |                  |                |      |            |                  |      |
|                                 | Status quo | Future situation |                |      |            |                  |      |
| PE120                           | 107148,1   | 107148,1         | PE             |      |            |                  |      |
| Treatment capacity              | 207000     | 207000           | PE             |      |            |                  |      |
| Electric energy consumption     |            |                  | Standard Range |      | Norm. (%)  |                  |      |
|                                 | Status quo | Future situation |                |      | Status quo | Future situation |      |
| Mechanical pre-treatment        | 5,876      | -                | kWh/PE120 y    | 2,5  | 5,5        | 112,5            | -    |
| Pumping stations                | 4,480      | -                | kWh/PE120 y    | 1,5  | 3,5        | 149,0            | -    |
| Screen                          | 1,397      | -                | kWh/PE120 y    | 0,5  | 1          | 179,3            | -    |
| Sand trap and primary clarifier | NA         | -                | kWh/PE120 y    | 0,5  | 1          | NA               | -    |
| Mechanical-biological treatment | 13,108     | -                | kWh/PE120 y    | 14,5 | 33         | -7,5             | -    |
| Aeration                        | 8,210      | -                | kWh/PE120 y    | 11,5 | 22         | -31,3            | -    |
| Stirrers                        | 2,190      | -                | kWh/PE120 y    | 1,5  | 4,5        | 23,0             | -    |
| Return sludge pumps             | 2,708      | -                | kWh/PE120 y    | 1    | 4,5        | 48,8             | -    |
| Miscellaneous (sec. clarifier)  | NA         | -                | kWh/PE120 y    | 0,5  | 2          | NA               | -    |
| Sludge treatment                | 4,149      | -                | kWh/PE120 y    | 2    | 7          | 43,0             | -    |
| Thickening                      | 1,540      | -                | kWh/PE120 y    | 0,5  | 1          | 207,9            | -    |
| Digestion                       | 0,838      | -                | kWh/PE120 y    | 1    | 2,5        | -10,8            | -    |
| Dewatering                      | 1,771      | -                | kWh/PE120 y    | 0,5  | 3,5        | 42,4             | -    |
| Infrastructure                  | NA         | -                | kWh/PE120 y    | 1    | 4,5        | NA               | -    |
| Heating                         | NA         | -                | kWh/PE120 y    | 0    | 2,5        | NA               | -    |
| Misc. infrastructure            | NA         | -                | kWh/PE120 y    | 1    | 2          | NA               | -    |
| Tot. elect. ener. consumption   | 23,134     | 23,134           | kWh/PE120 y    | 20   | 50         | 10,4             | 10,4 |

Initial inspection shows that plant has electric consumption inside the estimated range.

Biomethane unit installation instead of commonly operated CHP is evaluated by REEF2W tool.

| Energy from waste                             |            |                  |                   |
|---|------------|------------------|-------------------|
| Anaerobic digestion                           |            |                  |                   |
|   | Status quo | Future situation |                   |
| Total biogas production from AD               | 914789     | 914789           | m <sup>3</sup> /y |
| Digestate                                     | 44732,25   | 44732,25         | t/y               |
| Solid fraction after solid/liquid separator   | 43837,61   | 43837,61         | t/y               |
| Liquid fraction after solid/liquid separator  | 894,65     | 894,65           | t/y               |
| CHP installed power                           | 952,91     | NA               | kW                |
| Electric energy production from CHP           | 1854624    | NA               | kWh/y             |
| Thermal energy production from CHP            | 2132817    | NA               | kWh/y             |
| Electric energy consumption from biogas prod. | 22255,49   | NA               | kWh/y             |
| Thermal energy consumption from biogas prod.  | 106640,85  | NA               | kWh/y             |
| Electric energy consumption from Hydrolysis   | NA         | NA               | kWh/y             |
| Thermal energy consumption from Hydrolysis    | NA         | NA               | kWh/y             |
| Total biomethane production from Upgrading    | NA         | 546129,03        | m <sup>3</sup> /y |
| Electric energy consumption from Upgrading    | NA         | 311028,26        | kWh/y             |
| Fraction of biogas fed into the Upgrading     | NA         | 100,00           | %                 |
| Total methane production from PtG             | NA         | NA               | kWh/y             |
| Input power from PtG                          | NA         | NA               | kW                |

Current WWTP self-sufficiency is about 74%. Biomethane unit installation causes that no energy (both thermal and electrical) for self-consumption will be produced.



|  |           |       |
|--|-----------|-------|
| Electric energy PRODUCTION from Status Quo                 | 1854,624  | MWh/y |
| Electric energy CONSUMPTION from Status Quo                | 2500,970  | MWh/y |
| Remaining electric energy shortage/excess from Status Quo  | -646,346  | MWh/y |
| Electric energy PRODUCTION from Future Situation           | 0,000     | MWh/y |
| Electric energy CONSUMPTION from Future Situation          | 2789,743  | MWh/y |
| Remaining electric energy shortage/excess Future Situation | -2789,743 | MWh/y |

Because of no excess heat or electric energy production, there was no Spatial Assessment provided.

Environmental Assessment gives better output for CO<sub>2</sub>eq production for biomethane production.

| <b>Environment Assessment</b>    |            |                                 |
|----------------------------------|------------|---------------------------------|
| Carbon footprint/credit for:     | Status Quo | Future situation                |
| Imported electricity             | 445,98     | 1924,92 t CO <sub>2</sub> -eq   |
| Imported heat                    | NA         | NA t CO <sub>2</sub> -eq        |
| Aerobic treatment                | 961965,82  | 961965,82 t CO <sub>2</sub> -eq |
| Sludge handling                  | 21,30      | 21,30 t CO <sub>2</sub> -eq     |
| CHP engine and flare emissions   | 95,23      | NA t CO <sub>2</sub> -eq        |
| Exported electricity             | NA         | NA t CO <sub>2</sub> -eq        |
| Exported heat                    | NA         | NA t CO <sub>2</sub> -eq        |
| Methane slip during upgrading    | NA         | NA t CO <sub>2</sub> -eq        |
| Injected biomethane              | NA         | -1306,26 t CO <sub>2</sub> -eq  |
| Sludge use                       | -1397,86   | -1397,86 t CO <sub>2</sub> -eq  |
| <b>Carbon footprint scenario</b> | <b>NA</b>  | <b>NA</b> t CO <sub>2</sub> -eq |

For economic assessment, there are issues with the rentability of biomethane plant. There is significant rise of electric and heat consumption at the WWTP (no energy from CHP). These costs are not specified by REEF2W tool.

| <b>Economic Assessment</b>                        |           |          |
|---|-----------|----------|
| <b>Operating cost</b>                             |           |          |
| Biogas upgrading                                  | 216145,14 | EUR/year |
| Thermal Hydrolysis                                | 0,00      | EUR/year |
| PtG   | 0,00      | EUR/year |
| Heat pump   | 0,00      | EUR/year |
| Hydroelectric microturbine                        | 0,00      | EUR/year |
| Photovoltaic                                      | 0,00      | EUR/year |
| Thermal collector                                 | 0,00      | EUR/year |
| Hybrid PV/T collector                             | 0,00      | EUR/year |
| Pyrolysis   | 0,00      | EUR/year |
| Total operating cost                              | 216145,14 | EUR/year |
| <b>Investment cost</b>                            |           |          |
| Biogas upgrading                                  | 644005,42 | EUR      |
| Thermal Hydrolysis                                | 0,00      | EUR      |
| PtG   | 0,00      | EUR      |
| Heat pump   | 0,00      | EUR      |
| Hydroelectric microturbine                        | 0,00      | EUR      |
| Photovoltaic                                      | 0,00      | EUR      |
| Thermal collector                                 | 0,00      | EUR      |
| Hybrid PV/T collector                             | 0,00      | EUR      |
| Pyrolysis   | 0,00      | EUR      |
| Total investment cost                             | 644005,42 | EUR      |
| <b>Additional incomes</b>                         |           |          |
| Incomes/Expenditure - additional waste processing | 0,00      | EUR/year |
| Incomes from utilisation of heat                  | 0,00      | EUR/year |
| Incomes from utilisation of electricity           | 0,00      | EUR/year |
| Incomes biomethane selling into the grid          | 472932,89 | EUR/year |
| Incomes biomethane selling CNG                    | 0,00      | EUR/year |
| <b>Indicators</b>                                 |           |          |
| Return of the investment                          | 2,51      | Year     |
| Additional income                                 | 472932,89 | EUR      |
| Electrical Energy cost saving                     | 0,00      | EUR      |

The economic assessment gives a very good result. The return of investment is very good for RE project. The main issue is, that The Tool not validated the rise of costs of operation of the plant in case of stopping the operation of the CHP. The CHP is the best solution for the WWTP

Zlin operation. Biogas production is sufficient for all heat consumption at WWTP and 74% of electricity consumption. There is no excess biogas production for biomethane plant and replacing CHP with biomethane unit is not effective both energetically and economically.

## HRADEC KRALOVE

The plant situation was analyzed by REEF2W Tool with the following results:

| WWTP Description                 |                            |                  |                     |
|----------------------------------|----------------------------|------------------|---------------------|
|                                  | Status quo                 | Future situation |                     |
| Plant type                       | Wastewater Treatment Plant |                  |                     |
| Name of User                     | Hradec Králové             |                  |                     |
| Date                             | 2020/04/01                 |                  |                     |
| Country                          | Czech Republic             |                  |                     |
| Treatment capacity               | 141000                     | 141000           | PE (*)              |
| Connected population             | 121876                     | 121876           | PE (*)              |
| Daily average of wastewater flow | 33089                      | 33089            | m <sup>3</sup> /d   |
| COD inflow concentration         | 442                        | 442              | mg/l                |
| TN in influent                   | 38,45                      | 38,45            | kgTN/m <sup>3</sup> |

| Substrate                                 |            |                |              |
|---|------------|----------------|--------------|
| Status quo                                |            |                |              |
|   | Tons (t/y) | Tot. Solid (%) | Volatile (%) |
| Primary Sludge                            | 42653,0    | 4,6            | 67,6         |
| Secondary Sludge                          | 48399,0    | 2,4            | 70,8         |
| External Sewage Sludge                    | NA         | NA             | NA           |
| Organic Fraction of Municipal Solid Waste | NA         | NA             | NA           |
| Other                                     | 9427,0     | 50,0           | 50,0         |
| Other                                     | 1271,0     | 100,0          | 80,0         |
| Other                                     | 231,0      | 22,0           | 90,0         |
| NA  | NA         | NA             | NA           |

There is no change for substrate composition between the status quo and the future situation.

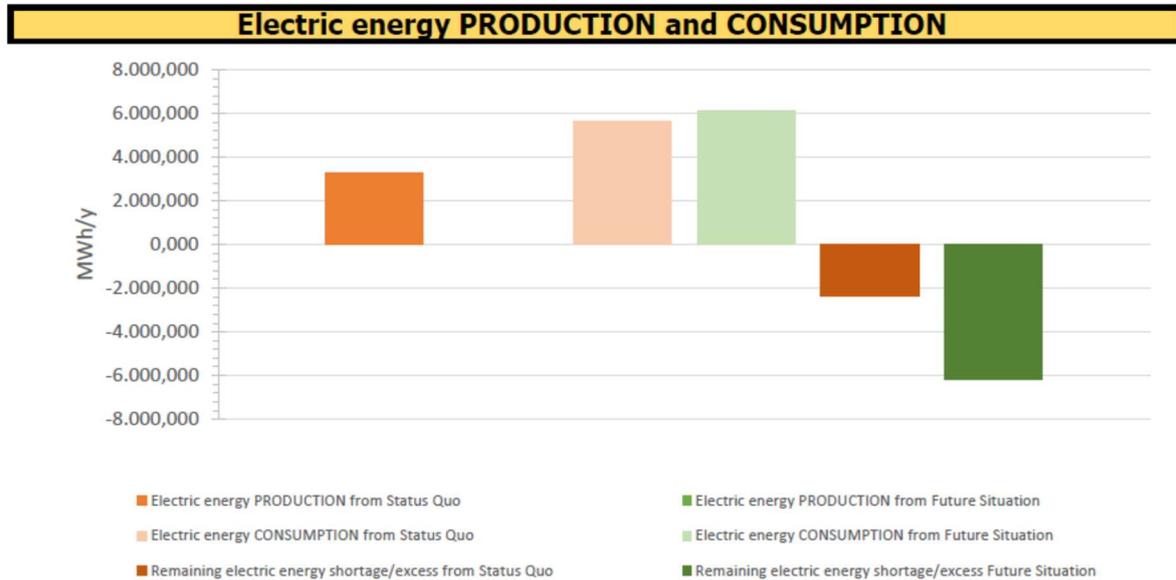
| Energy efficiency               |            |                  |                |      |            |                  |      |
|---------------------------------|------------|------------------|----------------|------|------------|------------------|------|
| WWTP Indicator                  |            |                  |                |      |            |                  |      |
|                                 | Status quo | Future situation |                |      |            |                  |      |
| PE120                           | 121877,8   | 121877,8         | PE             |      |            |                  |      |
| Treatment capacity              | 141000     | 141000           | PE             |      |            |                  |      |
| Electric energy consumption     |            |                  | Standard Range |      | Norm. (%)  |                  |      |
|                                 | Status quo | Future situation |                |      | Status quo | Future situation |      |
| Mechanical pre-treatment        | 17,070     | -                | kWh/PE120 y    | 2,5  | 5,5        | 485,7            | -    |
| Pumping stations                | 14,537     | -                | kWh/PE120 y    | 1,5  | 3,5        | 651,8            | -    |
| Screen                          | 2,534      | -                | kWh/PE120 y    | 0,5  | 1          | 406,7            | -    |
| Sand trap and primary clarifier | NA         | -                | kWh/PE120 y    | 0,5  | 1          | NA               | -    |
| Mechanical-biological treatment | 24,749     | -                | kWh/PE120 y    | 14,5 | 33         | 55,4             | -    |
| Aeration                        | 16,268     | -                | kWh/PE120 y    | 11,5 | 22         | 45,4             | -    |
| Stirrers                        | 1,258      | -                | kWh/PE120 y    | 1,5  | 4,5        | -8,1             | -    |
| Return sludge pumps             | 5,855      | -                | kWh/PE120 y    | 1    | 4,5        | 138,7            | -    |
| Miscellaneous (sec. clarifier)  | 1,369      | -                | kWh/PE120 y    | 0,5  | 2          | 57,9             | -    |
| Sludge treatment                | 4,154      | -                | kWh/PE120 y    | 2    | 7          | 43,1             | -    |
| Thickening                      | NA         | -                | kWh/PE120 y    | 0,5  | 1          | NA               | -    |
| Digestion                       | 1,300      | -                | kWh/PE120 y    | 1    | 2,5        | 20,0             | -    |
| Dewatering                      | 2,854      | -                | kWh/PE120 y    | 0,5  | 3,5        | 78,5             | -    |
| Infrastructure                  | NA         | -                | kWh/PE120 y    | 1    | 4,5        | NA               | -    |
| Heating                         | NA         | -                | kWh/PE120 y    | 0    | 2,5        | NA               | -    |
| Misc. infrastructure            | NA         | -                | kWh/PE120 y    | 1    | 2          | NA               | -    |
| Tot. elect. ener. consumption   | 45,973     | 45,973           | kWh/PE120 y    | 20   | 50         | 86,6             | 86,6 |

Initial inspection shows that plant electric consumption is in the standard range but at high value. The reason is high pumping station consumption and tertial treatment.

Biomethane unit installation instead of commonly operated CHP is evaluated by REEF2W tool.

| Energy from waste                             |            |                  |       |
|---|------------|------------------|-------|
| Anaerobic digestion                           |            |                  |       |
|   | Status quo | Future situation |       |
| Total biogas production from AD               | 1604650    | 1604650          | m3/y  |
| Digestate                                     | 100055,42  | 100055,42        | t/y   |
| Solid fraction after solid/liquid separator   | 98054,31   | 98054,31         | t/y   |
| Liquid fraction after solid/liquid separator  | 2001,11    | 2001,11          | t/y   |
| CHP installed power                           | 1671,51    | NA               | kW    |
| Electric energy production from CHP           | 3297000    | NA               | kWh/y |
| Thermal energy production from CHP            | 4582969    | NA               | kWh/y |
| Electric energy consumption from biogas prod. | 39564,00   | NA               | kWh/y |
| Thermal energy consumption from biogas prod.  | 229148,45  | NA               | kWh/y |
| Electric energy consumption from Hydrolysis   | NA         | NA               | kWh/y |
| Thermal energy consumption from Hydrolysis    | NA         | NA               | kWh/y |
| Total biomethane production from Upgrading    | NA         | 957976,05        | m3/y  |
| Electric energy consumption from Upgrading    | NA         | 545581,00        | kWh/y |
| Fraction of biogas fed into the Upgrading     | NA         | 100,00           | %     |
| Total methane production from PtG             | NA         | NA               | kWh/y |
| Input power from PtG                          | NA         | NA               | kW    |

The current WWTP self-sufficiency is about 58,4%. Biomethane unit installation causes that no energy (both thermal and electrical) for self-consumption will be produced.



|  |           |       |
|--|-----------|-------|
| Electric energy PRODUCTION from Status Quo                 | 3297,000  | MWh/y |
| Electric energy CONSUMPTION from Status Quo                | 5642,679  | MWh/y |
| Remaining electric energy shortage/excess from Status Quo  | -2345,679 | MWh/y |
| Electric energy PRODUCTION from Future Situation           | 0,000     | MWh/y |
| Electric energy CONSUMPTION from Future Situation          | 6148,696  | MWh/y |
| Remaining electric energy shortage/excess Future Situation | -6148,696 | MWh/y |

Because of no excess heat or electric energy production, there was no Spatial Assessment provided. There are also no development, industrial or residential areas as energy consumers in the distance to 3 km from WWTP.

Environmental Assessment gives better output for CO<sub>2</sub>eq production for biomethane production.

## Environment Assessment

| Carbon footprint/credit for:     | Status Quo        | Future situation  |        |
|----------------------------------|-------------------|-------------------|--------|
| Imported electricity             | 1618,52           | 4242,60           | CO2-eq |
| Imported heat                    | 634853,50         | 635872,30         | CO2-eq |
| Aerobic treatment                | 1160948,25        | 1160948,25        | CO2-eq |
| Sludge handling                  | 76,24             | 76,24             | CO2-eq |
| CHP engine and flare emissions   | 167,04            | NA                | CO2-eq |
| Exported electricity             | NA                | NA                | CO2-eq |
| Exported heat                    | NA                | NA                | CO2-eq |
| Methane slip during upgrading    | NA                | NA                | CO2-eq |
| Injected biomethane              | NA                | -2291,35          | CO2-eq |
| Sludge use                       | -5003,24          | -5003,24          | CO2-eq |
| <b>Carbon footprint scenario</b> | <b>1792660,31</b> | <b>1793844,79</b> | CO2-eq |

For economic assessment, there are issues with the rentability of biomethane plant. There is significant rise of electric and heat consumption at the WWTP (no energy from CHP). These costs are not specified by REEF2W tool.

| <b>Economic Assessment</b>                        |            |          |
|---|------------|----------|
| <b>Operating cost</b>                             |            |          |
| Biogas upgrading                                  | 368832,94  | EUR/year |
| Thermal Hydrolysis                                | 0,00       | EUR/year |
| PtG   | 0,00       | EUR/year |
| Heat pump   | 0,00       | EUR/year |
| Hydroelectric microturbine                        | 0,00       | EUR/year |
| Photovoltaic                                      | 0,00       | EUR/year |
| Thermal collector                                 | 0,00       | EUR/year |
| Hybrid PV/T collector                             | 0,00       | EUR/year |
| Pyrolysis   | 0,00       | EUR/year |
| Total operating cost                              | 368832,94  | EUR/year |
| <b>Investment cost</b>                            |            |          |
| Biogas upgrading                                  | 1009065,04 | EUR      |
| Thermal Hydrolysis                                | 0,00       | EUR      |
| PtG   | 0,00       | EUR      |
| Heat pump   | 0,00       | EUR      |
| Hydroelectric microturbine                        | 0,00       | EUR      |
| Photovoltaic                                      | 0,00       | EUR      |
| Thermal collector                                 | 0,00       | EUR      |
| Hybrid PV/T collector                             | 0,00       | EUR      |
| Pyrolysis   | 0,00       | EUR      |
| Total investment cost                             | 1009065,04 | EUR      |
| <b>Additional incomes</b>                         |            |          |
| Incomes/Expenditure - additional waste processing | 0,00       | EUR/year |
| Incomes from utilisation of heat                  | 0,00       | EUR/year |
| Incomes from utilisation of electricity           | 0,00       | EUR/year |
| Incomes biomethane selling into the grid          | 565623,55  | EUR/year |
| Incomes biomethane selling CNG                    | 0,00       | EUR/year |
| <b>Indicators</b>                                 |            |          |
| Return of the investment                          | 5,13       | Year     |
| Additional income                                 | 565623,55  | EUR      |
| Electrical Energy cost saving                     | 0,00       | EUR      |

The CHP is the best solution for WWTP Hradec Kralove operation. Biogas production is sufficient for all heat consumption at WWTP and 58,4% of electricity consumption. There is no excess biogas production for biomethane plant and replacing CHP with biomethane unit is not effective both energetically and economically.

OLOMOUC

The plant situation was analyzed by REEF2W Tool with following results:

| WWTP Description                 |                            |                  |                     |
|----------------------------------|----------------------------|------------------|---------------------|
|                                  | Status quo                 | Future situation |                     |
| Plant type                       | Wastewater Treatment Plant |                  |                     |
| Name of User                     | Olomouc                    |                  |                     |
| Date                             | 2020/04/01                 |                  |                     |
| Country                          | Czech Republic             |                  |                     |
| Treatment capacity               | 259500                     | 259500           | PE (*)              |
| Connected population             | 180295                     | 180295           | PE (*)              |
| Daily average of wastewater flow | 27387                      | 27387            | m <sup>3</sup> /d   |
| COD inflow concentration         | 790                        | 790              | mg/l                |
| TN in influent                   | 61,8                       | 61,8             | kgTN/m <sup>3</sup> |

| Substrate                                 |            |                |              |
|---|------------|----------------|--------------|
| Status quo                                |            |                |              |
|   | Tons (t/y) | Tot. Solid (%) | Volatile (%) |
| Primary Sludge                            | 79546,0    | 3,4            | 74,9         |
| Secondary Sludge                          | 45494,0    | 5,4            | 67,9         |
| External Sewage Sludge                    | NA         | NA             | NA           |
| Organic Fraction of Municipal Solid Waste | NA         | NA             | NA           |
| Other                                     | 1050,0     | 100,0          | 92,0         |
| NA  | NA         | NA             | NA           |
| NA  | NA         | NA             | NA           |
| NA  | NA         | NA             | NA           |

There are no changes for substrates in comparison to the status quo and future situation.

## Energy efficiency

| WWTP Indicator     |  | Status quo | Future situation |
|--------------------|--|------------|------------------|
| PE120              |  | 180297,8   | 180297,8 PE      |
| Treatment capacity |  | 259500     | 259500 PE        |

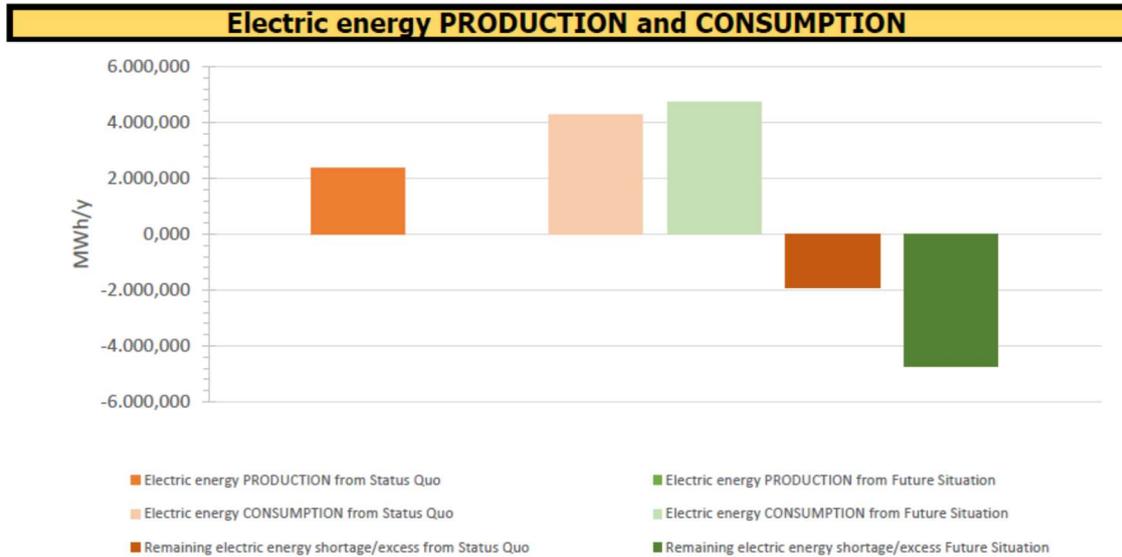
| Electric energy consumption     |            |                  |             | Norm. (%)      |            |                  |      |
|---------------------------------|------------|------------------|-------------|----------------|------------|------------------|------|
|                                 | Status quo | Future situation |             | Standard Range | Status quo | Future situation |      |
| Mechanical pre-treatment        | 3,682      | -                | kWh/PE120 y | 2,5            | 5,5        | 39,4             | -    |
| Pumping stations                | NA         | -                | kWh/PE120 y | 1,5            | 3,5        | NA               | -    |
| Screen                          | 3,682      | -                | kWh/PE120 y | 0,5            | 1          | 636,5            | -    |
| Sand trap and primary clarifier | NA         | -                | kWh/PE120 y | 0,5            | 1          | NA               | -    |
| Mechanical-biological treatment | 17,052     | -                | kWh/PE120 y | 14,5           | 33         | 13,8             | -    |
| Aeration                        | 13,618     | -                | kWh/PE120 y | 11,5           | 22         | 20,2             | -    |
| Stirrers                        | 2,138      | -                | kWh/PE120 y | 1,5            | 4,5        | 21,3             | -    |
| Return sludge pumps             | 1,296      | -                | kWh/PE120 y | 1              | 4,5        | 8,4              | -    |
| Miscellaneous (sec. clarifier)  | NA         | -                | kWh/PE120 y | 0,5            | 2          | NA               | -    |
| Sludge treatment                | 2,850      | -                | kWh/PE120 y | 2              | 7          | 17,0             | -    |
| Thickening                      | 1,288      | -                | kWh/PE120 y | 0,5            | 1          | 157,5            | -    |
| Digestion                       | 0,500      | -                | kWh/PE120 y | 1              | 2,5        | -33,3            | -    |
| Dewatering                      | 1,063      | -                | kWh/PE120 y | 0,5            | 3,5        | 18,8             | -    |
| Infrastructure                  | NA         | -                | kWh/PE120 y | 1              | 4,5        | NA               | -    |
| Heating                         | NA         | -                | kWh/PE120 y | 0              | 2,5        | NA               | -    |
| Misc. infrastructure            | NA         | -                | kWh/PE120 y | 1              | 2          | NA               | -    |
| Tot. elect. ener. consumption   | 23,585     | 23,585           | kWh/PE120 y | 20             | 50         | 11,9             | 11,9 |

Initial inspection shows that plant has low electric consumption at the expected range.

Biomethane unit installation instead of commonly operated CHP is evaluated by REEF2W tool.

| Energy from waste                             |            |                  |                   |
|---|------------|------------------|-------------------|
| Anaerobic digestion                           |            |                  |                   |
|   | Status quo | Future situation |                   |
| Total biogas production from AD               | 1355895    | 1355895          | m <sup>3</sup> /y |
| Digestate                                     | 124462,93  | 124462,93        | t/y               |
| Solid fraction after solid/liquid separator   | 121973,67  | 121973,67        | t/y               |
| Liquid fraction after solid/liquid separator  | 2489,26    | 2489,26          | t/y               |
| CHP installed power                           | 1412,39    | NA               | kw                |
| Electric energy production from CHP           | 2368455    | NA               | kWh/y             |
| Thermal energy production from CHP            | 4425858    | NA               | kWh/y             |
| Electric energy consumption from biogas prod. | 28421,46   | NA               | kWh/y             |
| Thermal energy consumption from biogas prod.  | 221292,90  | NA               | kWh/y             |
| Electric energy consumption from Hydrolysis   | NA         | NA               | kWh/y             |
| Thermal energy consumption from Hydrolysis    | NA         | NA               | kWh/y             |
| Total biomethane production from Upgrading    | NA         | 809469,32        | m <sup>3</sup> /y |
| Electric energy consumption from Upgrading    | NA         | 461004,30        | kWh/y             |
| Fraction of biogas fed into the Upgrading     | NA         | 100,00           | %                 |
| Total methane production from PtG             | NA         | NA               | kWh/y             |
| Input power from PtG                          | NA         | NA               | kw                |

Current WWTP self-sufficiency is about 45,3%. Biomethane unit installation causes, that no energy (both thermal and electrical) for self-consumption will be produced.



|  |           |       |
|--|-----------|-------|
| Electric energy PRODUCTION from Status Quo                 | 2368,455  | MWh/y |
| Electric energy CONSUMPTION from Status Quo                | 4280,671  | MWh/y |
| Remaining electric energy shortage/excess from Status Quo  | -1912,216 | MWh/y |
| Electric energy PRODUCTION from Future Situation           | 0,000     | MWh/y |
| Electric energy CONSUMPTION from Future Situation          | 4713,254  | MWh/y |
| Remaining electric energy shortage/excess Future Situation | -4713,254 | MWh/y |

Because of no excess heat or electric energy production, there was no Spatial Assessment provided.

Environmental Assessment gives better output for CO<sub>2</sub>eq production for biomethane production.

**Environment Assessment**

| Carbon footprint/credit for:     | Status Quo        | Future situation  |                            |
|----------------------------------|-------------------|-------------------|----------------------------|
| Imported electricity             | 1319,43           | 3252,15           | t CO <sub>2</sub> -eq      |
| Imported heat                    | NA                | NA                | t CO <sub>2</sub> -eq      |
| Aerobic treatment                | 1544421,40        | 1544421,40        | t CO <sub>2</sub> -eq      |
| Sludge handling                  | 52,04             | 52,04             | t CO <sub>2</sub> -eq      |
| CHP engine and flare emissions   | 141,15            | NA                | t CO <sub>2</sub> -eq      |
| Exported electricity             | NA                | NA                | t CO <sub>2</sub> -eq      |
| Exported heat                    | NA                | NA                | t CO <sub>2</sub> -eq      |
| Methane slip during upgrading    | NA                | NA                | t CO <sub>2</sub> -eq      |
| Injected biomethane              | NA                | -1936,14          | t CO <sub>2</sub> -eq      |
| Sludge use                       | -3415,04          | -3415,04          | t CO <sub>2</sub> -eq      |
| <b>Carbon footprint scenario</b> | <b>1542518,97</b> | <b>1542374,40</b> | <b>t CO<sub>2</sub>-eq</b> |

For economic assessment, there are issues with the rentability of biomethane plant. There is significant rise of electric and heat consumption at the WWTP (no energy from CHP). These costs are not specified by REEF2W tool.

| <b>Economic Assessment</b>                        |           |          |
|---|-----------|----------|
| <b>Operating cost</b>                             |           |          |
| Biogas upgrading                                  | 314797,80 | EUR/year |
| Thermal Hydrolysis                                | 0,00      | EUR/year |
| PtG   | 0,00      | EUR/year |
| Heat pump   | 0,00      | EUR/year |
| Hydroelectric microturbine                        | 0,00      | EUR/year |
| Photovoltaic                                      | 0,00      | EUR/year |
| Thermal collector                                 | 0,00      | EUR/year |
| Hybrid PV/T collector                             | 0,00      | EUR/year |
| Pyrolysis   | 0,00      | EUR/year |
| Total operating cost                              | 314797,80 | EUR/year |
| <b>Investment cost</b>                            |           |          |
| Biogas upgrading                                  | 889383,23 | EUR      |
| Thermal Hydrolysis                                | 0,00      | EUR      |
| PtG   | 0,00      | EUR      |
| Heat pump   | 0,00      | EUR      |
| Hydroelectric microturbine                        | 0,00      | EUR      |
| Photovoltaic                                      | 0,00      | EUR      |
| Thermal collector                                 | 0,00      | EUR      |
| Hybrid PV/T collector                             | 0,00      | EUR      |
| Pyrolysis   | 0,00      | EUR      |
| Total investment cost                             | 889383,23 | EUR      |
| <b>Additional incomes</b>                         |           |          |
| Incomes/Expenditure - additional waste processing | 0,00      | EUR/year |
| Incomes from utilisation of heat                  | 0,00      | EUR/year |
| Incomes from utilisation of electricity           | 0,00      | EUR/year |
| Incomes biomethane selling into the grid          | 477939,82 | EUR/year |
| Incomes biomethane selling CNG                    | 0,00      | EUR/year |
| <b>Indicators</b>                                 |           |          |
| Return of the investment                          | 5,45      | Year     |
| Additional income                                 | 477939,82 | EUR      |
| Electrical Energy cost saving                     | 0,00      | EUR      |

The CHP seems to be an optimal solution for WWTP Olomouc operation. Biogas production is sufficient for all heat consumption at WWTP and 58,4% of electricity consumption. There is

no excess biogas production for biomethane plant and replacing CHP with biomethane unit seems to be not effective enough both energetically and economically.

Now the municipality has to take a decision on further biogas utilization. The presented pre-assessment was performed using the REEF2W tool and elaboration of a feasibility study can be used as a crucial basis for the selection of an optimal and sustainable solution.

## **D) CONCLUSION**

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There were three large municipal WWTP operated by Veolia chosen for preassessment. At these plants, there were long-time multiple parameters benchmarking provided, so there are operational data available. Plants are mechanical/biological WWTPs with anaerobic digestion step. Biogas is used for electricity and heat production by CHP (gas engines).

Plants are evaluated by REEF2W Tool and the possibility of installing the biomethane production unit was validated.

All three plants have electric consumption in the range expected by the REEF2W tool. Power consumption at Zlin and Olomouc Plant is significantly lower than at Hradec Kralove. The reason is higher pumping consumption at Hradec (high altitude of pumping) and tertiary treatment.

Biomethane unit has a better environmental impact but economically is often better to use CHP because the produced energy is used for self-consumption of WWTP.

At Olomouc plant, now the further biogas utilization is evaluated. It is necessary to replace old CHP engines. Evaluated solutions were boiler connected to sludge dryer, biomethane unit, and new CHP.

As the most promising plant for performing a feasibility study (D.T4.3.5.) was finally selected WWTP Olomouc, because of the high interest of the municipality of Olomouc city and the utility Moravská vodárenská a.s., which is the operator of the plant.